

Print ISSN: 2423-673X

Online ISSN: 2423-6721



Dissociation Enthalpy of Methane/Carbon dioxide/Nitrogen and Tetra nbutylammonium Chloride Semiclathrate Hydrates Using the Clausius-**Clapeyron Equation**

Abolfazl Mohammadi * 💿, Mohmmad Aryaeipanah 💿, Maryam Hakimizadeh 💿

- 1. Department of Chemical Engineering, University of Bojnord, Bojnord, Iran. E-mail: mohammadi.a@ub.ac.ir
- 2. Department of Chemical Engineering, University of Bojnord, Bojnord, Iran. E-mail: aryaeipanahmohammad2022@gmail.com
- 3. Department of Chemical Engineering, University of Bojnord, Bojnord, Iran. E-mail: maryamhakimizadehboj32@gmail.com

ARTICLE INFO	ABSTRACT
Article History:	Due to high storage capacity, high dissociation enthalpy, and the
Received: 10 December 2021	appropriate melting point of gas hydrates, these compounds have the
Revised: 10 January 2022	potential for many industrial applications. Tetra-n-butylammonium halides
Accepted: 12 January 2022	are molecules that can form semiclathrate hydrates. This manuscript
- ·	employed the Clausius Clapeyron equation to evaluate the dissociation
Article type: Research	enthalpy of methane/nitrogen/carbon dioxide + tetra-n-butylammonium
	chloride (TBAC) semiclathrate hydrates (SCHs). Phase equilibrium data
Keywords:	are measured in a batch reactor with an effective volume of 460 cc. The data
Clausius-Clapeyron,	of dissociation enthalpy were evaluated in the temperatures of (275.15 to
Dissociation Enthalpy,	304.75) K and the pressures of (0.36 to 10.57) MPa at (0 - 0.36) mass
Gas Hydrates,	fraction of TBAC. The results showed that the utilization of TBAC
Semiclathrates,	increases the amount of dissociation enthalpy of semiclathrate hydrates per
Tetra-n-Butylammonium	mole of the hydrated gas. By increasing the amount of TBAC in the system,
Chloride	the quantity of dissociation enthalpy per mole of hydrated gas increased.

Introduction

Gas hydrates (also called clathrate hydrates) are solid ice-like structures that form from water and gas. These compounds are formed when "guest" molecules such as hydrogen sulfide, methane, ethane, carbon dioxide, nitrogen, etc. Their shape and size are appropriate and placed into the hydrogen bond cavities in the lattice of water molecules (host) through van der Waals forces. High pressures and low temperatures are the required thermodynamic conditions to form clathrate hydrates [1].

Structure sI, structure sII, and structure sH are well-known structures of clathrate hydrates [2, 3]. Because of the relatively high storage capacity of gas hydrates (filled gas hydrates can release about 180 STP volumes of the gas per the unit volume of formed gas hydrate), high dissociation/formation enthalpy, and proper melting point, these materials can be used in many industries such as the transportation of natural gas [4-7], water desalination industries [8-11], gas separation applications [6, 12-14], gas storage industries [15-17], and storage of cold energy in air conditioning systems [18-22]. Therefore, finding the hydrate formers with moderate

Journal of Chemical and Petroleum Engineering, 2022, 56 (1): 123-131.

Publisher: University of Tehran, College of Engineering DOI: 10.22059/JCHPE.2022.335066.1373 © Abolfazl Mohammadi, Mohmmad Aryaeipanah, Maryam Hakimizadeh



^{*} Corresponding Author: A. Mohammadi (E-mail address: mohammadi.a@ub.ac.ir)



hydrate formation conditions and high dissociation enthalpy is favorable for the industrialization of hydrate-based technologies.

Understanding the phase behaviors and formation/dissociation enthalpies of gas hydrates is of great importance for developing hydrate-based technologies. Sun and coworkers calculated the formation/dissociation enthalpy of methane hydrates in salt solutions using Clapeyron and Clausius-Clapeyron equations [23]. The calculated dissociation enthalpies by the Clapeyron equation did not show temperature dependence, while the calculated values obtained by the Clausius-Clapeyron equation decreased with the temperature increase [23]. Experimental investigations performed by Kang and coworkers on the formation/dissociation enthalpies of methane/carbon dioxide hydrates at 273.15 K showed that the dissociation/formation enthalpy of these clathrate hydrates are 362.64 kJ/kg and 471.54 kJ/kg, respectively. The measured data shows that the amount of the formation/dissociation enthalpies of methane/carbon dioxide hydrates is higher than the amount of ice latent melting heat (334 kJ/kg) [24].

Recently, the researchers have employed some quaternary ammonium salts as hydrate former [25-29]. Tetra-n-butylammonium halides (TBAX) such as tetra-n-butylammonium bromide (TBAB), tetra-n-butylammonium chloride (TBAC) or tetra-n-butylammonium fluoride (TBAF) are typical guest molecule that can form the semiclathrate hydrates. The structure of semiclathrate compounds is different from the well-known structures of gas hydrates. In the common gas hydrate structures (sI, sII, and sH), guest molecules occupy the cages formed by the host water molecules. While, in semiclathrate hydrate structures, a part of the used semiclathrate former (halide ions) participates in the lattice structure of the cages along with water molecules. In this type of hydrate, tetra-n-butylammonium cations (TBA⁻) occupy the large cavities and the small cavities can be occupied by appropriate gas molecules such as carbon dioxide, nitrogen, and methane [30].

Deschamps and Dalmazzone measured the formation/dissociation enthalpies of nitrogen/carbon dioxide + TBAB semiclathrate hydrates using the under pressure differential scanning calorimetry (DSC) method [31]. The results of these researchers showed that the formation/dissociation enthalpies of TBAB + gas semiclathrate hydrates increase by increasing the pressure [31]. In another study, Sugahara and Machida measured the formation/dissociation enthalpy of TBAB semiclathrate hydrates at high pressures [32]. Their experimental results showed that the formation/dissociation enthalpy of TBAB semiclathrate hydrates at high pressures [32]. Their experimental results showed that the formation/dissociation enthalpy of TBAB·26H₂O is about (192 ± 3) J·g^{-1,} and this amount is almost constant at the pressures of up to 800 bar [32]. In 2008, Delahaye and Fournaison studied the formation/dissociation enthalpies of (carbon dioxide + TBAB) semiclathrate hydrates using the differential thermal analysis (DTA) method. They experimentally showed that the formation/dissociation enthalpy of formed (carbon dioxide +TBAB) double hydrates is about 313.2 kJ kg⁻¹ in the presence of 9 wt% TBAB at the pressure of 2 MPa [33].

The phase behaviors and dissociation enthalpies of SCHs formed in the presence of semiclathrate formers are not well known. There are two common methods to obtain the formation/dissociation enthalpies of gas hydrates. Calorimetric determination is the first method that is a direct method of measurement. and indirect calculation using the. Employing the well-known equations such as Clapeyron or Clausius–Clapeyron equations along with phase equilibrium data is the second method to obtain the formation/dissociation enthalpies. In this research, the formation/dissociation enthalpies of (methane/nitrogen/carbon dioxide + TBAC) SCHs are determined by Clausius–Clapeyron equation.

Experimental

Materials and Device

TBAC with a purity of 0.95 mass fraction was purchased from Merck. The purities and suppliers of all materials used in this work are given in Table 1.

Javidani et al. [34], Mohammadi et al. [35], and Abedi et al. [36] have described the experimental device used in this research. Fig. 1 depicts the schematic diagram of the used experimental apparatus in this research. The effective volume of the used reactor is 460 cc. The reactor is equipped with two ball valves for injecting/discharging the aqueous solution and two needle valves to inject/discharge the methane/carbon dioxide/nitrogen. Controlling the temperature of the reactor is done by a water/ethylene glycol circulator. The speed of the rocking-cell reactor is set at 10 rpm.

Table 1. Purities and suppliers of materials used in this work					
Chemical Name	Supplier	Purity			
TBAC ^a	Merck	0.95 mass fraction			
methane	Varian Gas	0.99995 mol fraction			
nitrogen	Varian Gas	0.9995 mol fraction			
carbon dioxide	Varian Gas	0.999 mol fraction			

^a TBAC= tetra n-butyl ammonium chloride



Fig. 1. Schematic illustration of the experimental apparatus

Procedure

After washing the inner part of the reactor with distilled water, a PLATINUM® vacuum pump is employed to evacuate the air inside the reactor. 100 cc aqueous solutions of TBAC with various concentrations ((0 - 0.36) mass) fraction are prepared and injected into the reactor. The gas cylinder is connected to the cell, and the desired gas (methane/nitrogen/carbon dioxide) is injected into the reactor. Then, the electromotor is tautened on. The agitation of the solution



is performed with a rocking-cell speed of 25 rpm. After colling and then heating the solution, the equilibrium data is obtained.

Results and Discussion

The formation/dissociation enthalpies of gas hydrates / semiclathrate hydrates are a significant parameter to consider these compounds as a possible source for storing the energy. In the work, the enthalpy of dissociation/formation is obtained by determining the slope of Ln(p) vs. 1/T curves using the Clausius - Clapeyron equation [37]. After measuring the equilibrium data of TBAC + methane/nitrogen/carbon dioxide semiclathrate hydrates, Clausius-Clapeyron equation [37] (Eq. 1) was employed to calculate the dissociation/formation enthalpy of double methane/nitrogen/carbon dioxide + TBAC SCHs.

$$\frac{d\ln p}{d(1/T)} = \frac{-\Delta H_{diss}}{z.R}$$
(1)

where ΔH_{diss} stands for dissociation/formation enthalpy in kJ/mole. *p* and *T*, respectively, are pressure in MPa and the temperature in kelvin (K). *z* is the mean value of the compressibility factor over the ranges of *T* and *P* under study (calculate using Peng-Robinson (PR) equation of state [38]) and *R* is gas constant.

Figs. 2 to 4 show the Clapeyron p-T phase diagram of semiclathrate hydrate phase equilibrium for methane/nitrogen/carbon dioxide + TBAC + water systems. The straight lines in these figures demonstrate the best linear fit of the empirical data. As can be seen in these figures, the obtained straight lines fitted from experimental data show good agreement with experimental data, which validates the assumptions related to the Clausius-Clapeyron equation.



Fig. 2. Clapeyron p-T phase diagram of semiclathrate hydrate phase equilibrium for TBAC + methane + water system. The straight lines represent the best linear fit of the experimental data



Fig. 3. Clapeyron p-T phase diagram of semiclathrate hydrate phase equilibrium for TBAC + carbon dioxide + water system. The straight lines represent the best linear fit of the experimental data

Calculated mean values of compressibility factor and molar dissociation enthalpies (ΔH_{diss}) of TBAC + methane/nitrogen/carbon dioxide double semiclathrate hydrates (kJ/mol) are presented in Table 2. Dissociation enthalpies per mole of hydrated gas are shown in Fig. 5. As shown in Table 2 and Fig. 5 the dissociation enthalpy of gas + TBAC double semiclathrate hydrate per mol of hydrated gas increases by increasing the mass fraction of TBAC. The higher enthalpies of hydrate dissociation in higher mass fractions of TBAC indicate that more energy is required to trap the gas molecules inside the cavities at higher TBAC concentrations.



Fig. 4. Clapeyron p-T phase diagram of semiclathrate hydrate phase equilibrium for TBAC + nitrogen + water system. The straight lines represent the best linear fit of the experimental data



WTBAX	System	ΔH _{diss} / kJ/mol	Z	Reference
	·	gas		
	Water + TBAC + Methane			
0		58.80	0.8595	[39]
0.05		161.00	0.8767	[39]
0.1		168.43	0.9254	[40]
0.15		184.26	0.8790	[39]
0.2		202.49	0.9322	[41]
0.22		238.24	0.8964	[39]
0.3		315.44	0.9371	[41]
0.34		337.95	0.9328	[42]
	Water + TBAC + Carbon dioxide			
0		65.33	0.7762	[39]
0.0434		216.95	0.8555	[43]
0.0874		276.31	0.8468	[43]
0.15		343.01	0.7838	[39]
0.22		335.32	0.8283	[39]
0.34		356.92	0.8384	[42]
0.3618		381.52	0.9169	[44]
	Water + TBAC + Nitrogen			
297.7	_	77.78	1.1754	[45]
0.15		339.44	0.9796	[39]
0.22		429.98	0.9816	[39]
0.34		1082.08	0.9878	[42]

Table 2. Calculate	ed mean values of c	ompressibility	factor and n	nolar dissociatior	enthalpies (ΔH_{diss})	of TBAC +
	methane/nitrogen/	carbon dioxide	double semi	iclathrate hydrate	es (kJ/mol _{gas})	



Fig. 5. Dissociation enthalpy of semiclathrate hydrates for the systems of TBAC + methane/nitrogen/carbon dioxide + water versus the mass fraction of TBAC

The amounts of dissociation/formation enthalpies of gas hydrates in the presence of TBAC show that the formed semiclathrate hydrates in the presence of nitrogen have a higher quantity

of ΔH_{diss} in comparison with carbon dioxide and methane. This may be due to the low tendency of nitrogen to be trapped in small cavities of formed semiclathrate hydrates.

Conclusion

The amounts of dissociation enthalpies of methane/nitrogen/carbon dioxide + TBAC semiclathrate hydrates were calculated using the Clausius-Clapeyron equation. The calculated dissociation enthalpy of gas + TBAC double semiclathrate hydrate per mol of hydrated gas increased by increasing the mass fraction of TBAC. Nitrogen + TBAC semiclathrate hydrates had higher dissociation enthalpy per mol of hydrated gas compared to carbon dioxide and methane.

Acknowledgment

This work has been supported by the center of International Scientific Studies & Collaborations (CISSC), the ministry of science research and technology.

References

- [1] Sloan JED, Koh KA. Clathrate Hydrates of Natural Gases. 3rd ed. ed: CRC Press, Taylor & Francis Group, 2008.
- [2] Khokhar A, Gudmundsson J, Sloan E. Gas storage in structure H hydrates. Fluid Phase Equilibria. 1998;150:383-92.
- [3] Sloan D. Natural Gas Hydrates in Flow Assurance. Boston: Gulf Professional Publishing; 2011.
 p. 1-11.
- [4] Wu Q, Yu Y, Zhang B, Gao X, Zhang Q. Effect of temperature on safety and stability of gas hydrate during coal mine gas storage and transportation. Safety Science. 2019;118:264-72.
- [5] Chaturvedi E, Prasad N, Mandal A. Enhanced formation of methane hydrate using a novel synthesized anionic surfactant for application in storage and transportation of natural gas. Journal of Natural Gas Science and Engineering. 2018;56:246-57.
- [6] Hassan H, Javidani AM, Mohammadi A, Pahlavanzadeh H, Abedi-Farizhendi S, Mohammadi AH. Effects of Graphene Oxide Nanosheets and Al2O3 Nanoparticles on CO2 Uptake in Semiclathrate Hydrates. Chemical Engineering & Technology. 2021;44(1):48-57.
- [7] Mohammadi A, Fazli RH, Asil AG. Influence of Tetra n-Butylammonium Chloride and Polysorbate 80 on the Kinetics of Methane Hydrate Formation. Journal of the Japan Petroleum Institute. 2021;64(1):22-8.
- [8] Fakharian H, Ganji H, Naderifar A, Mofrad HR, Kakavand M. Effect of gas type and salinity on performance of produced water desalination using gas hydrates. Journal of Water Reuse and Desalination. 2019.
- [9] Babu P, Nambiar A, He T, Karimi IA, Lee JD, Englezos P, et al. A review of clathrate hydrate based desalination to strengthen energy–water nexus. ACS Sustainable Chemistry & Engineering. 2018;6(7):8093-107.
- [10] Linga P, Babu P, Nambiar A. Effect of NaCl on clathrate hydrate based desalination HyDesal process with fixed bed approach. Conference Effect of NaCl on clathrate hydrate based desalination HyDesal process with fixed bed approach, vol. 2018. Hamad bin Khalifa University Press (HBKU Press), p. EEPP1035.
- [11] Pahlavanzadeh H, Javidani AM, Ganji H, Mohammadi A. Investigation of the Effect of NaCl on the Kinetics of R410a Hydrate Formation in the Presence and Absence of Cyclopentane with Potential Application in Hydrate-based Desalination. Industrial & Engineering Chemistry Research. 2020;59(31):14115-25.
- [12] Dashti H, Lou X. Gas Hydrate-Based CO 2 Separation Process: Quantitative Assessment of the Effectiveness of Various Chemical Additives Involved in the Process. Conference Gas Hydrate-Based CO 2 Separation Process: Quantitative Assessment of the Effectiveness of Various Chemical Additives Involved in the Process. Springer, p. 3-16.



- [13] Warrier P, Naveed Khan M, Carreon MA, Peters CJ, Koh CA. Integrated gas hydrate-membrane system for natural gas purification. Journal of Renewable and Sustainable Energy. 2018;10(3):034701.
- [14] Gupta P, Sangwai JS. Semiclathrate Hydrate of Methane and Quaternary Ammonium Salts for Natural Gas Storage and Gas Separation. Conference Semiclathrate Hydrate of Methane and Quaternary Ammonium Salts for Natural Gas Storage and Gas Separation. Offshore Technology Conference.
- [15] Veluswamy HP, Kumar A, Seo Y, Lee JD, Linga P. A review of solidified natural gas (SNG) technology for gas storage via clathrate hydrates. Applied Energy. 2018;216:262-85.
- [16] Kiran BS, Sowjanya K, Prasad PS, Yoon J-H. Experimental investigations on tetrahydrofuranmethane-water system: Rapid methane gas storage in hydrates. Oil & Gas Science and Technology-Revue d'IFP Energies nouvelles. 2019;74:12.
- [17] Kumar A, Veluswamy HP, Kumar R, Linga P. Rapid Methane Storage in Seawater Via Clathrate Hydrates. Available at SSRN 3212833. 2018.
- [18] Delahaye A, Fournaison L, Dalmazzone D. Use of Hydrates for Cold Storage and Distribution in Refrigeration and Air-Conditioning Applications. Gas Hydrates 2: Geoscience Issues and Potential Industrial Applications. 2018:315-58.
- [19] Mohammadi A, Jodat A. Investigation of the kinetics of TBAB+ carbon dioxide semiclathrate hydrate in presence of tween 80 as a cold storage material. Journal of Molecular Liquids. 2019;293:111433.
- [20] Xie N, Tan C, Yang S, Liu Z. Conceptual design and analysis of a novel CO2 hydrate-based refrigeration system with cold energy storage. ACS Sustainable Chemistry & Engineering. 2018;7(1):1502-11.
- [21] Mohammadi A. The roles TBAF and SDS on the kinetics of methane hydrate formation as a cold storage material. Journal of Molecular Liquids. 2020;309:113175.
- [22] Javidani AM, Abedi-Farizhendi S, Mohammadi A, Mohammadi AH, Hassan H, Pahlavanzadeh H. Experimental study and kinetic modeling of R410a hydrate formation in presence of SDS, tween 20, and graphene oxide nanosheets with application in cold storage. Journal of Molecular Liquids. 2020;304:112665.
- [23] Sun S, Zhao J, Yu D. Dissociation enthalpy of methane hydrate in salt solution. Fluid Phase Equilibria. 2018;456:92-7.
- [24] Kang S-P, Lee H, Ryu B-J. Enthalpies of dissociation of clathrate hydrates of carbon dioxide, nitrogen,(carbon dioxide+ nitrogen), and (carbon dioxide+ nitrogen+ tetrahydrofuran). The Journal of Chemical Thermodynamics. 2001;33(5):513-21.
- [25] Sugahara T, Machida H, Muromachi S, Tenma N. Thermodynamic properties of tetra-nbutylammonium 2-ethylbutyrate semiclathrate hydrate for latent heat storage. International Journal of Refrigeration. 2019;106:113-9.
- [26] Shi L, Liang D. Semiclathrate hydrate phase behaviour and structure for CH4 in the presence of tetrabutylammonium fluoride (TBAF). The Journal of Chemical Thermodynamics. 2019;135:252-9.
- [27] Shimada M, Shimada J, Sugahara T, Tsunashima K. Phase equilibrium relations for tetra-nbutylphosphonium acetate semiclathrate hydrate systems in the presence of methane, carbon dioxide, nitrogen, or ethane. Fluid Phase Equilibria. 2019;488:48-53.
- [28] Ilani-Kashkouli P, Hashemi H, Basdeo A, Naidoo P, Ramjugernath D. Hydrate Dissociation Data for the Systems (CO2/CH4/Ar)+ Water with (TBAF/TBAA/TBPB/TBANO3 and Cyclopentane). Journal of Chemical & Engineering Data. 2019.
- [29] Shi L, Yi L, Shen X, Wu W, Liang D. Dissociation Temperatures of Mixed Semiclathrate Hydrates Formed with Tetrabutylammonium Bromide Plus Tetrabutylammonium Chloride. Journal of Chemical & Engineering Data. 2016;61(6):2155-9.
- [30] Sangwai JS, Oellrich L. Phase equilibrium of semiclathrate hydrates of methane in aqueous solutions of tetra-n-butyl ammonium bromide (TBAB) and TBAB–NaCl. Fluid Phase Equilibria. 2014;367:95-102.

- [31] Deschamps J, Dalmazzone D. Dissociation enthalpies and phase equilibrium for TBAB semiclathrate hydrates of N2, CO2, N2+ CO2 and CH4+ CO2. Journal of thermal analysis and calorimetry. 2009;98(1):113-8.
- [32] Sugahara T, Machida H. Dissociation and Nucleation of Tetra-n-butyl Ammonium Bromide Semi-Clathrate Hydrates at High Pressures. Journal of Chemical & Engineering Data. 2017;62(9):2721-5.
- [33] Lin W, Delahaye A, Fournaison L. Phase equilibrium and dissociation enthalpy for semiclathrate hydrate of CO2+TBAB. Fluid Phase Equilibria. 2008;264(1):220-7.
- [34] Javidani AM, Abedi-Farizhendi S, Mohammadi A, Hassan H, Mohammadi AH, Manteghian M. The effects of graphene oxide nanosheets and Al2O3 nanoparticles on the kinetics of methane+ THF hydrate formation at moderate conditions. Journal of Molecular Liquids. 2020;316:113872.
- [35] Mohammadi A, Manteghian M, Haghtalab A, Mohammadi AH, Rahmati-Abkenar M. Kinetic study of carbon dioxide hydrate formation in presence of silver nanoparticles and SDS. Chemical Engineering Journal. 2014;237:387-95.
- [36] Abedi-Farizhendi S, Iranshahi M, Mohammadi A, Manteghian M, Mohammadi AH. Kinetic study of methane hydrate formation in the presence of carbon nanostructures. Petroleum Science. 2019;16(3):657-68.
- [37] Sloan E, Fleyfel F. Hydrate dissociation enthalpy and guest size. Fluid Phase Equilibria. 1992;76:123-40.
- [38] Peng DY, Robinson DB. A New two Constant Equation of State. Ind Eng Chem Fundam. 1976;15:59-64.
- [39] Mohammadi A, Manteghian M, Mohammadi AH. Phase equilibria of semiclathrate hydrates for methane+ tetra n-butylammonium chloride (TBAC), carbon dioxide+ TBAC, and nitrogen+ TBAC aqueous solution systems. Fluid Phase Equilibria. 2014;381:102-7.
- [40] Kamran-Pirzaman A, Pahlavanzadeh H, Mohammadi AH. Hydrate phase equilibria of furan, acetone, 1, 4-dioxane, TBAC and TBAF. The Journal of Chemical Thermodynamics. 2013;64:151-8.
- [41] Sun Z-G, Liu C-G. Equilibrium conditions of methane in semiclathrate hydrates of tetra-nbutylammonium chloride. Journal of Chemical & Engineering Data. 2012;57(3):978-81.
- [42] Makino T, Yamamoto T, Nagata K, Sakamoto H, Hashimoto S, Sugahara T, et al. Thermodynamic Stabilities of Tetra-n-butyl Ammonium Chloride + H2, N2, CH4, CO2, or C2H6 Semiclathrate Hydrate Systems. Journal of Chemical & Engineering Data. 2010;55(2):839-41.
- [43] Li S, Fan S, Wang J, Lang X, Wang Y. Semiclathrate Hydrate Phase Equilibria for CO2 in the Presence of Tetra-n-butyl Ammonium Halide (Bromide, Chloride, or Fluoride). Journal of Chemical & Engineering Data. 2010;55(9):3212-5.
- [44] Mayoufi N, Dalmazzone D, Fürst W, Delahaye A, Fournaison L. CO2 Enclathration in Hydrates of Peralkyl-(Ammonium/Phosphonium) Salts: Stability Conditions and Dissociation Enthalpies. Journal of Chemical & Engineering Data. 2009;55(3):1271-5.
- [45] Van Cleeff A, Diepen GAM. Gas hydrates of nitrogen and oxygen. Recueil des Travaux Chimiques des Pays-Bas. 1960;79(6):582-6.

How to cite: Mohammadi A, Aryaeipanah M, Hakimizadeh M. Dissociation Enthalpy of Methane/Carbon dioxide/Nitrogen and Tetra n-butylammonium Chloride Semiclathrate Hydrates Using the Clausius-Clapeyron Equation. Journal of Chemical and Petroleum Engineering. 2022; 56(1): 123-131.